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**GB 2268276 A**

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(58) Field of Search

UK CL (Edition O ) **G1S SQA**

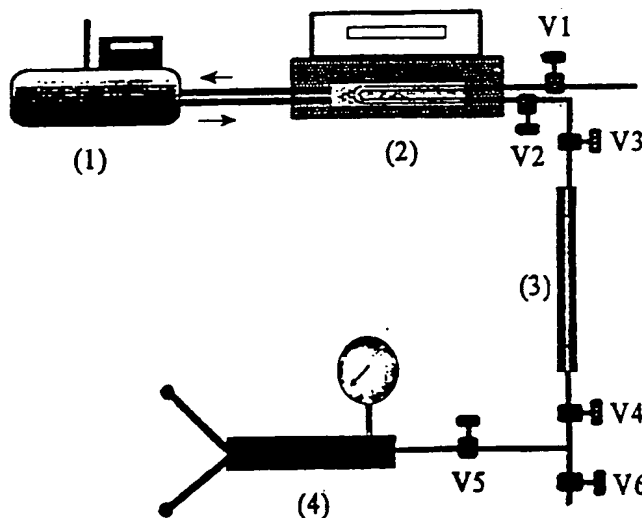
INT CL<sup>6</sup> **G01N 25/02 25/12 33/26 33/28 33/30**

On-line : **WPI**

(54) Method/apparatus for determining wax appearance temperature

(57) A method and apparatus for determining the wax appearance temperature of paraffinic petroleum oils comprises measuring and plotting the density of the paraffinic oil as a function of temperature at constant pressure, the wax appearance temperature being given by the inflexion point of the graph. The apparatus comprises an ultrathermostatic bath 1, a densimeter 2, a supply bottle 3, a mercury pump 4 and a valve system made up of valves V1 to V6 to link the circuit comprising the mercury pump, the supply bottle 3 and densimeter 2. The mercury pump is used to transfer fluid from the supply bottle 3 to the densimeter cell 2.

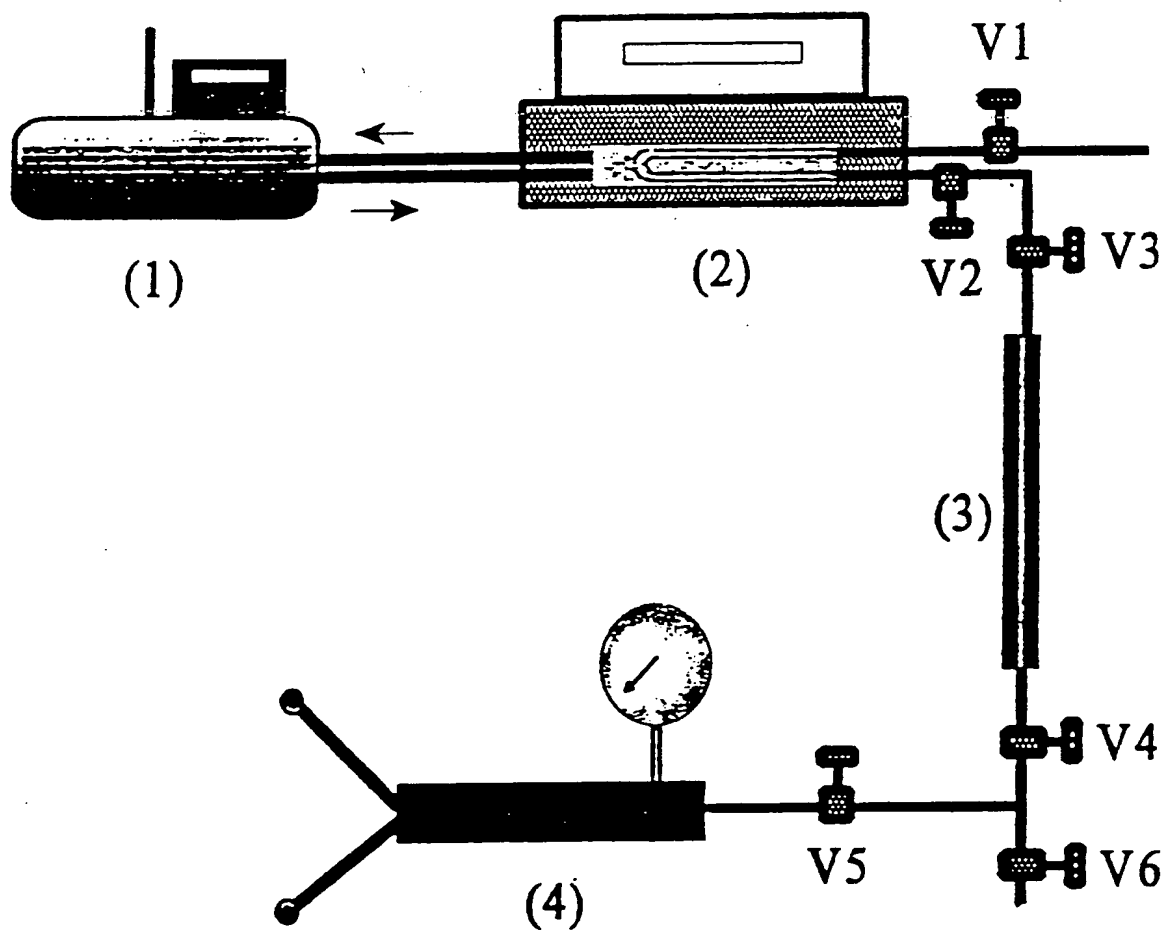
FIG. 1



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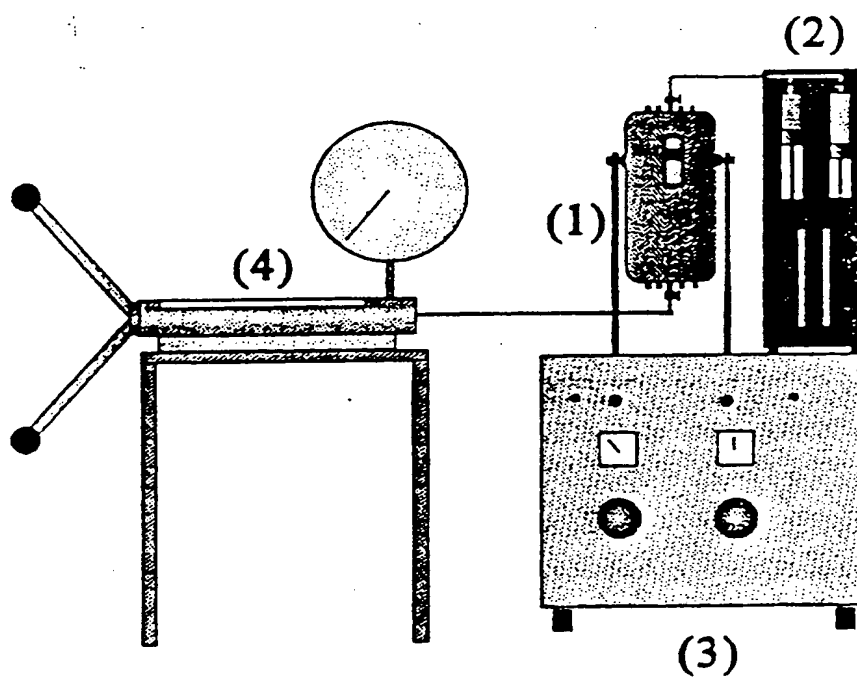
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FIG. 1



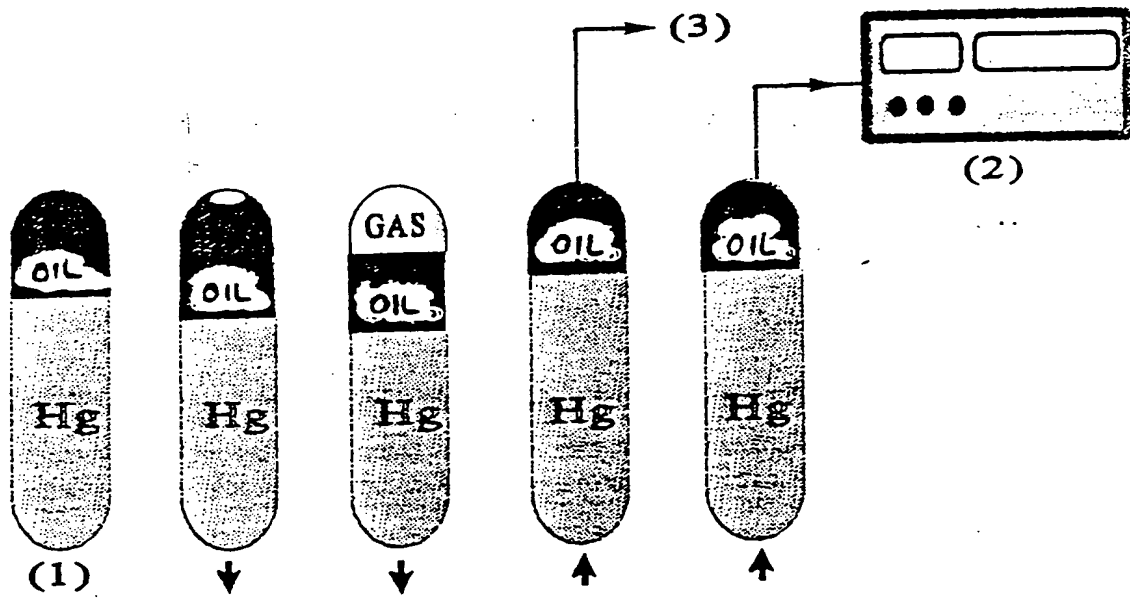
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FIG. 2



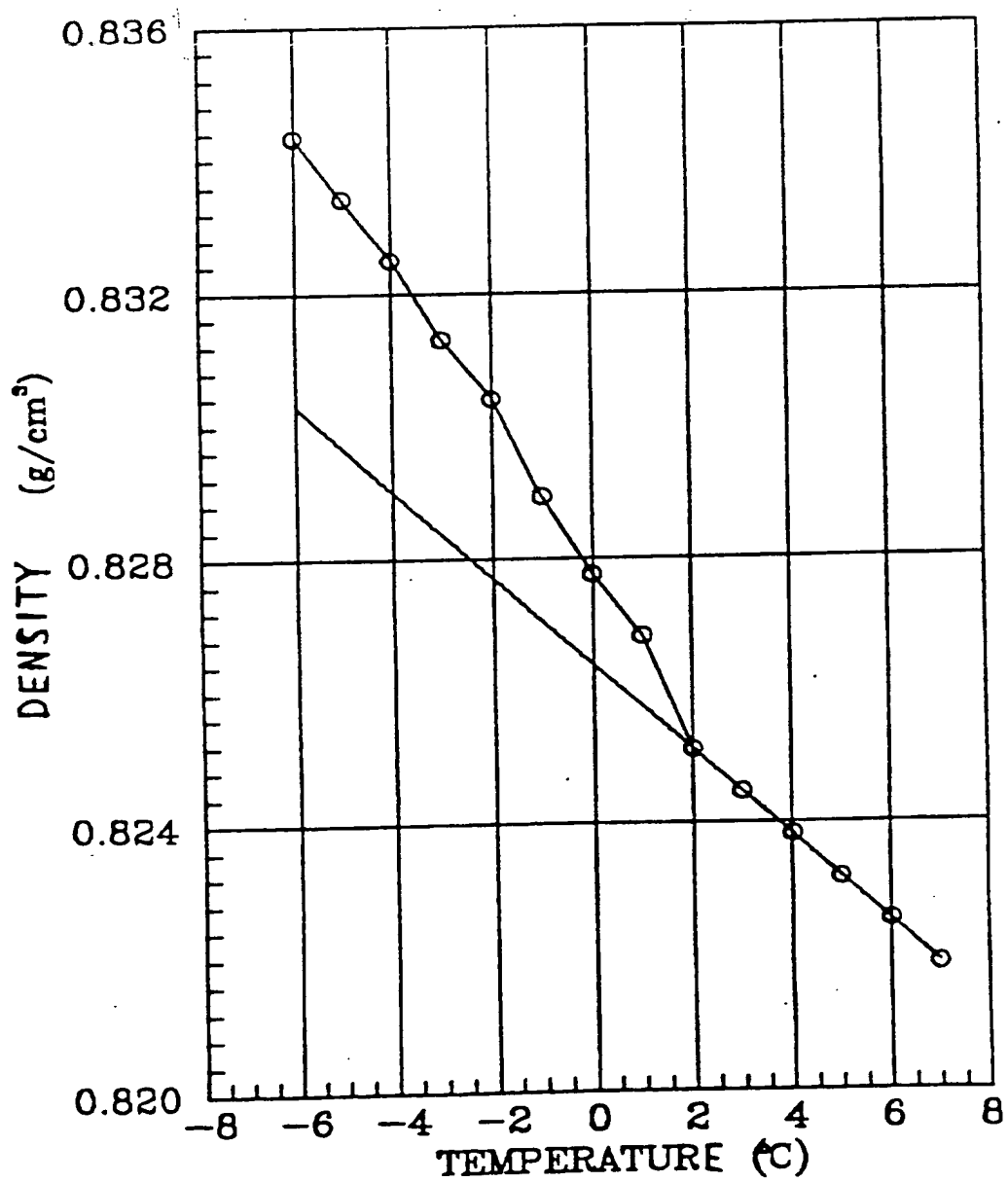
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FIG. 3



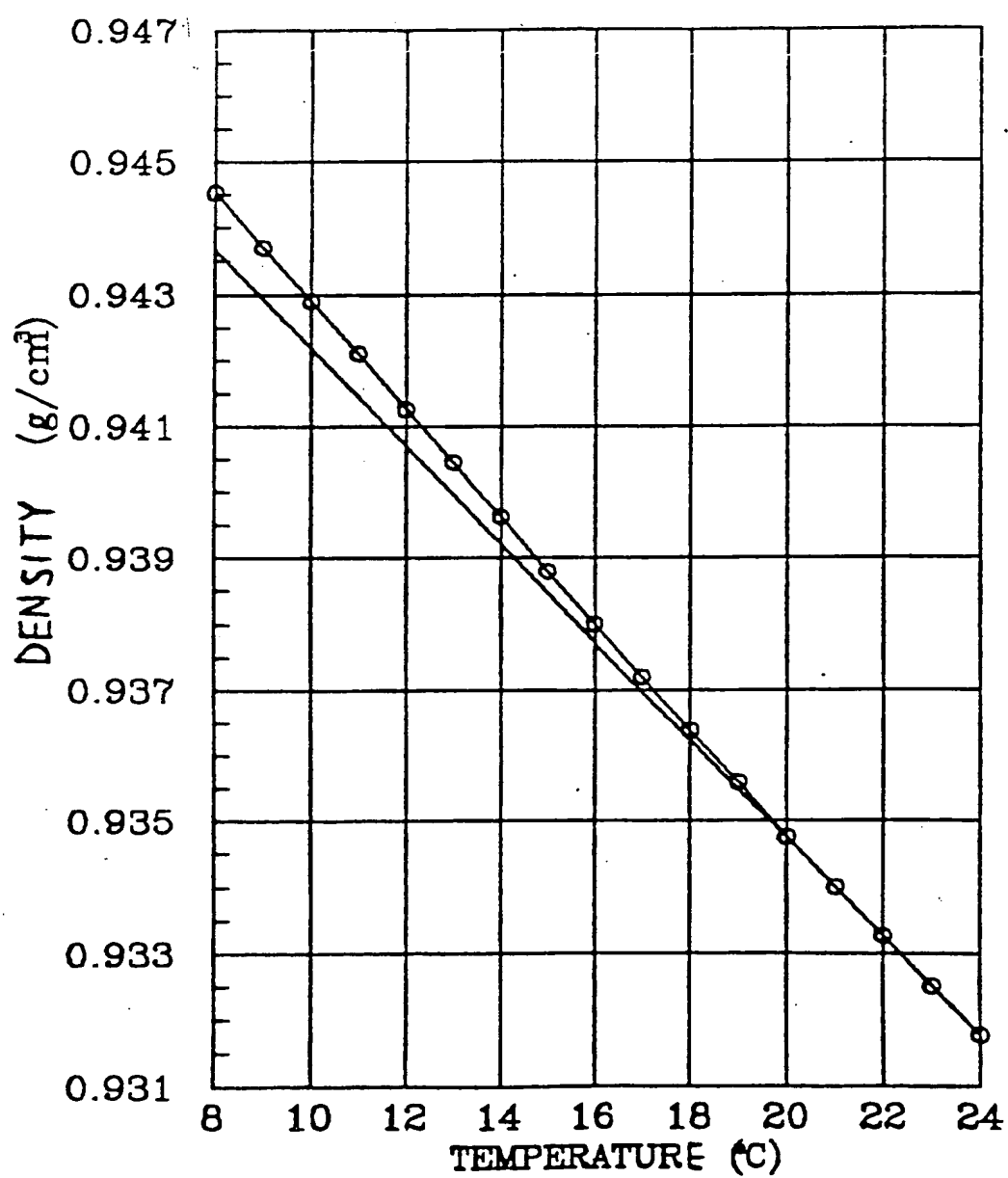
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FIG. 4



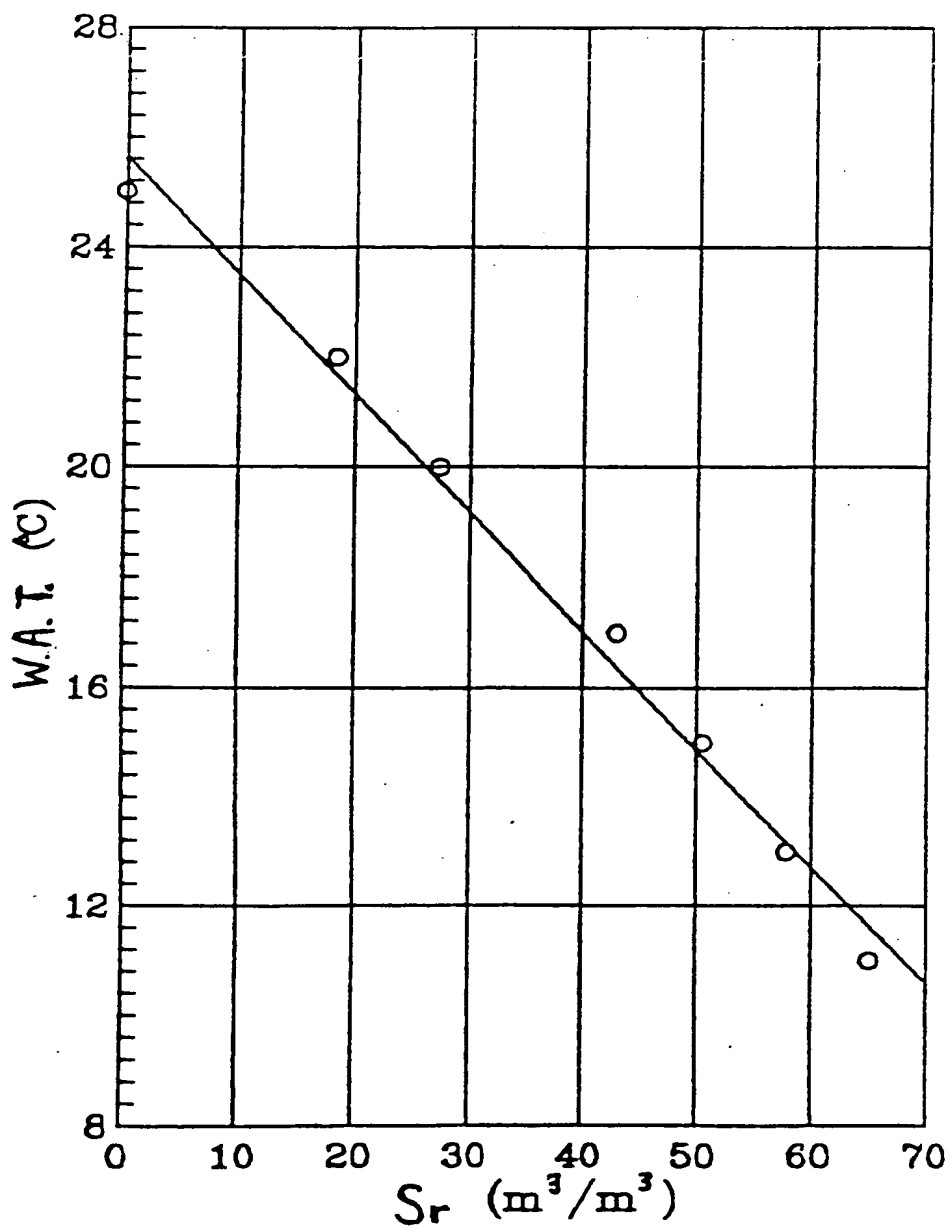
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FIG. 5



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FIG. 6





METHOD AND APPARATUS FOR DETERMINING THE WAX  
APPEARANCE TEMPERATURE OF PARAFFINIC PETROLEUM OILS

The present invention relates to a method and apparatus  
5 used to determine the wax appearance temperature or cloud point  
of waxy or paraffinic petroleum oils.

More specifically, the present invention concerns a  
method to determine the wax appearance temperature of  
paraffinic petroleum oils by measuring the change in density  
10 of the petroleum oil at the wax appearance temperature by means  
of a Pressure-Volume-Temperature (PVT) cell coupled to a high  
pressure and temperature densimeter.

Throughout the present specification, the terms  
"petroleum oils" and "fluid" represent hydrocarbon fluids as  
15 present in a reservoir, with or without gas dissolved therein.

Generally, the composition of oils and hydrocarbon fluids  
is of such complexity that it is difficult to estimate the  
number of components of such fluids. However, it is usual to  
consider the presence of straight-chained (n-paraffins) and  
20 branched paraffins (iso-paraffins), naphthenes (cycloparaffins)  
and aromatic compounds. Besides, there are further small  
amounts of compounds such as asphaltenes and resins which  
include heteroatoms and heavy metals.

It is also important to distinguish between dead oil  
25 (without gas) and live fluid (with gas, such as occurs in a  
reservoir). The content of light hydrocarbons ( $C_1$  to  $C_6$ ) in  
live fluid is in the order of 20 mol% higher than that for dead  
oil.

For the straight-chained paraffins, the change in  
30 physical properties is proportional with the increase in chain  
length. The branched paraffins have less predictable  
properties. An increasing level of branching will, in most  
cases, lead to a reduction in the boiling point and melting  
point. The composition of paraffins in each oil is a function  
35 of factors such as the geological origin of the oil. For wax  
appearance this means that it is very difficult to characterize  
the material appearing. The wax which appears will mainly be  
normal paraffins on account of the higher content of these  
components and because the melting points for n-paraffins are

considerably higher than for most other components in the oil. Models which are based on a wax fraction which is dissolved in the rest of the oil must therefore have a good analytical description of the composition of the complete fluid, in both  
5 its solid and liquid phases.

It is common knowledge that the content of light components in the fluid exerts an influence on the solubility of the longer chain components at a given temperature. Besides, the increase in pressure, as a function of a higher content in  
10 light components, will affect the properties of the components in the oil and thus also the solubility. Thus the overall effect of higher pressure and higher content of light components will depend on the total composition of the fluid.

On the other hand, the improvement in the exploration of  
15 paraffinic oil reservoirs necessarily involves a mathematical model which would represent the behaviour of such oils as concerns their flow in porous media and in pipelines, as well as the thermodynamic balance of the gas, liquid and solid phases, the latest phase having origin in the paraffins which  
20 crystallize out from solution.

The development of the model requires that the behaviour of the fluid, in some of the conditions where the real phenomenon occurs in the reservoir or in the pipelines, be known. Once this behaviour is adjusted, the model can be  
25 applied to effect simulations and determine the fluid behaviour in any condition.

To determine the wax appearance point or cloud point of an oil at different compositions, the influence of pressure on the wax appearance point, and a study on the reversibility of  
30 the process, are of paramount importance for the modelling of a paraffinic oil or a hydrocarbon fluid.

According to the ASTM Standard Test n° D2500-91 the wax appearance point is determined by the direct visualization of the formation of waxy or paraffinic crystals in the fluid  
35 within a transparent vessel kept in a controlled temperature bath. Because a mist or cloud is developed in the fluid, the wax appearance point is also known as its cloud point. The above mentioned ASTM Standard is limited to clear fluids.

In the technique known as Differential Scanning

Calorimetry (DSC) the measurement of the heat released during the solidification of the paraffin crystals is the basis for determining the cloud point. However, this technique can yield artificially low figures for the wax appearance point, mainly  
5 in the case of petroleum oils of low paraffin content.

In the optical microscopy process, the measurement of the wax appearance point is effected by detecting the appearance of the paraffin crystals on the thin layer of an optical microscope. This thin layer is coupled to a system of  
10 controlled cooling. The polarized light reaching the thin layer renders it easier to detect the onset of wax appearance. The preparation of a thin layer (50 $\mu$ m) and the incidence of light render it possible to use opaque fluids such as petroleum oils. While the optical microscopy method provides wax appearance  
15 points with reasonable accuracy, it is not a very practical method as an everyday, routine analytical tool.

In another approach, the viscosity is determined at several temperatures. The cloud point is identified by an inflexion on the curve of viscosity vs. temperature. As in the  
20 DSC technique, this technique can equally yield figures for wax appearance point which are lower than the real ones.

GB-A-2268276 describes a method of determining the wax appearance point in a petroleum product wherein the petroleum volume is measured and is plotted as a function of temperature  
25 at constant pressure, wherein the wax appearance point of the waxy or paraffinic phase occurs at the temperature at which there is a deviation in the graph. The method described in GB-A-2268276 comprises further determining the quantity of wax in a petroleum product at a particular temperature below the wax  
30 appearance point by (i) estimating the density of the solid and liquid wax, (ii) measuring the change in volume of the petroleum product due to the formation of solid wax phase, and (iii) multiplying the difference of the density of the wax in the two phases as determined by the measured volume change.

35 According to British GB-A-2268276 phase changes in the fluid derive from a temperature variation. The alleged advantage lies in the fact that the measurement of certain fluid properties can be directly explained by the transition from liquid phase to solid phase. The apparatus used in the

method of the British publication comprises a pressure cell placed in a thermostatic bath, a pump connected to the pressure cell to produce pressure, sensors to determine pressure, temperature and volume in the cell, and a control unit to read and set the cell pressure, temperature and volume.

However, it has been found that, since the accuracy of volumetric measurements by pumps such as the ones described in GB-A-2268276 is of  $0.01 \text{ cm}^3$ , then for a  $60 \text{ cm}^3$  sample described in Figure 2 of the publication the lowest detectable volume contraction is  $(0.01 \text{ cm}^3 \text{ in } 60 \text{ cm}^3) = 0.017 \%$ , this order of magnitude being present only for the wax appearance point of highly paraffinic oils. Thus, the method described in GB-A-2268276 is in practice limited to highly paraffinic oils. Besides there are drawbacks involved in preparing several samples each of  $60 \text{ cm}^3$ , having varying amounts of gas in order to vary the oil composition and thus to determine the influence of the composition on the wax appearance point. In order to determine the influence of the composition on the wax appearance point, it is necessary to have at least  $1000 \text{ cm}^3$  of oil which must be solubilized with varying amounts of gas.

Therefore there is the need for a method and high-precision apparatus to determine the wax appearance point of oils with a wide range of paraffinic contents, including contents as low as  $0.5 \text{ wt}\%$ , using small volume samples, the measurements being effected in short periods of time.

Accordingly one aspect of the present invention provides a method for determining the wax appearance temperature of paraffinic petroleum oils, comprising measuring and plotting the density of the petroleum oil as a function of the temperature at constant pressure, and determining the wax appearance point as the temperature at which there is an inflexion in the graph.

Thus, the method of the present invention comprises determining the temperature of wax appearance point of paraffin crystals of petroleum oils and related products, the oil being stabilized under atmospheric conditions (dead oil) or containing solubilized gas (live fluid).

Basically, the method of the present invention comprises measuring the density of the petroleum oil at various

temperatures and plotting the figures on a graph. Contrary to non-paraffinic oils where the behaviour of the density is practically linear at all temperatures, for oils showing some paraffinic content there is a portion of linear behaviour at higher temperatures and a portion, at lower temperatures, where the behaviour is no longer linear and an increase in density occurs as compared with the prolonging of the linear behaviour. The temperature where the linear behaviour ceases is considered as the temperature of the wax appearance point. The increase in density is associated to the shrinking of the fluid which is caused by the fact that paraffin molecules get nearer to each other during the wax appearance. The density of the fluid is measured using a high pressure and temperature densimeter.

The present invention comprises further determining the influence of the dissolved gas on the wax appearance point of pressurized fluids.

Thus the present invention provides a high precision method for determining the temperature of wax appearance point of oils with or without gas in solution (live fluid or dead oil respectively), the oils containing of from 0.5 weight % of waxes or paraffins, by measuring the change in density of the fluid as a function of temperature, by means of a high temperature and pressure densimeter.

Another objective is to determine the influence of the dissolved gas as quantified by the solubility ratio  $S_r$ , on the wax appearance point of pressurized fluids. For such purpose, the densimeter is coupled to a Pressure-Volume-Temperature cell which is an apparatus where a mercury piston permits that the pressure and the volume of the fluid within the cell be varied.

Still another objective is a high-precision apparatus for determining the wax appearance point of oils showing wax or paraffin content of from 0.5 wt % upwards, the oil having or not having gas dissolved therein (live fluid or dead oil respectively), the apparatus consisting basically of a vessel or bottle capable of withstanding pressure and temperature and which is coupled to a high-precision densimeter.

A second aspect of the invention provides apparatus for use in the method of the first aspect, which comprises a bottle to contain the sample of paraffinic oil, a mercury pump for

evacuating the bottle and a high pressure and temperature densimeter connected to the bottle for determining the variation in density of the sample with the temperature reduction, wherein the densimeter has its temperature regulated by an ultrathermostatic bath, and wherein the bottle, the mercury pump and the densimeter are connected together by a valve system.

In order that the present invention may more readily be understood the following description is given, merely by way of example, with reference to the accompanying drawings, in which:-

FIGURE 1 is a schematic view of an apparatus of this present invention to determine the wax appearance point of dead oils;

FIGURE 2 is a schematic view of a Pressure-Volume-Temperature cell;

FIGURE 3 shows schematically the combined Pressure-Volume-Temperature cell and densimeter for determining the wax appearance point as a function of the solubility ratio ( $S_r$ ) of the oil;

FIGURE 4 is a graph to determine the wax appearance point of a diesel oil fluid;

FIGURE 5 illustrates the inventive process for an oil containing as low as 0.5 weight % of waxes;

FIGURE 6 is a graph illustrating the influence of solubilized gas on the wax appearance point.

A preferred mode of carrying out the present invention is illustrated in FIGURE 1 where the wax appearance point is measured for a single petroleum oil composition, either dead or live fluid. The apparatus used to carry out the invention comprises an ultrathermostatic bath (1), a densimeter (2), a supply bottle (3), a mercury pump (4) and valve system made up of valves V1 to V6 to link the circuit comprising the mercury pump (4), the supply bottle (3) and the densimeter (2). The valve system comprises: densimeter outlet valve V1, densimeter inlet valve V2, top bottle valve V3, lower bottle valve V4, mercury pump connection valve V5, and supply valve V6. According to this operating mode of the invention the supply bottle (3) is a cylinder 0.8 cm in diameter and 25 cm high,

which yields a 20 cm volume. In this case the bottle (3) is evacuated and then filled through the valve V6.

In the other preferred mode of the present invention, that is, when the wax appearance point of a live fluid is to be determined, the bottle (3) is replaced by a bottle which already contains the fluid sample collected in the well oil under reservoir conditions (that is, high pressure and dissolved gas). This bottle is a cylinder 10 cm in diameter and 40 cm high, which yields a 600 cm<sup>3</sup> volume.

Initially, the ultrathermostatic bath is at a temperature which exceeds the wax appearance point by at least 20°C. The ultrathermostatic bath keeps the desired temperature of the densimeter cell within 0.1°C. Mercury pump (4) transfers fluid from supply bottle (3) to the densimeter cell (2), if necessary with heating. Readings of the oscillation period of the densimeter are effected every ten minutes, at intervals of 1°C, the ten minutes period being required for the stabilization of the system. The reading of the oscillation period is converted into a density value by means of the calibration equation of the densimeter. The densimeter is a commercial apparatus model ANTON PAAR DMA512 with which the density of a fluid (oil or gas) can be determined with a precision of 1.10<sup>-4</sup>g/cm<sup>3</sup> from the oscillation period of a U-shaped tube (the diapason principle). The natural frequency (f) of the system depends on the specific weight of the fluid contained within the tube (  $\rho_t$  ) where:

$$f = \frac{1}{T} = \frac{1}{2} \sqrt{\frac{C_1}{m_t + \rho_t v_t}}$$

wherein T is the temperature, C<sub>1</sub> is the gauging constant of the apparatus, and m<sub>t</sub> and v<sub>t</sub> are respectively the mass and the volume of the tube.

In this embodiment of the invention the influence of pressure on the wax appearance point of fluids having no dissolved gas can be ascertained. By closing the outlet valve V1 of the densimeter (2), the system can be pressurized to the desired pressure by means of the mercury pump (4) and measurements of the oscillation period at the desired

temperatures can be obtained.

As described hereinabove, the preferred embodiment of the present invention has accuracy and practicability as main advantages over the prior art processes such as Differential Scanning calorimetry and rheology or viscosity measuring. This stems from the fact that, being a static measurement, the behaviour of the density is more stable than that of viscosity, this latter depending on dynamic parameters. Besides, the densimeter makes it possible to measure density to the fourth decimal place, this accuracy being not reached by the apparatus of the prior art. The optical microscopy method, in spite of being fairly accurate, is not very practical for everyday purposes.

FIGURE 5 illustrates a preferred embodiment of the present invention as applied to a dead oil which contains as low as 0.5 wt % paraffins. While the prior art processes for such low-paraffin content oils are inconclusive, the high-precision method of the present invention easily yielded the desired value.

It should be understood that most of the methods for determining the wax appearance point of paraffinic petroleum oils cited in the literature are directed to dead oils, with no dissolved gas. However, using the wax appearance point of dead oils as a parameter in the designing of thermal recovery methods in paraffinic oil reservoirs, or in the designing of production installations (string, lines and separators), can be a drawback to the technical and economical feasibility studies of exploration projects. This is due to the fact that, determining the wax appearance point without taking into consideration the effect of light fractions dissolved in the petroleum oil, fails to represent the actual condition of the petroleum oil in question, since the light fractions dissolved therein increase the solubility of the waxes or paraffins in the liquid phase, therefore reducing the temperature at which the solid phase is formed (that is, the crystallization temperature). Therefore there is the need for a method which would be easy to perform and which would be directed to determining the live wax appearance point of an as-produced oil, this method and apparatus being provided by the present



invention.

Another preferred mode of the present invention is directed to determining the wax appearance point of as-produced oils, that is, petroleum oils containing dissolved gas. As  
5 illustrated in FIGURE 2, this preferred mode uses a Pressure-Volume-Temperature cell which comprises a metal cylinder (1) provided with controlled heating means (not shown in the Figure), a mechanical agitation system, and a glass window to observe the oil within the cell, a collecting means and  
10 measuring device (2) to determine the gas volume, a control panel (3) for controlling agitation and temperature, and a mercury pump (4) provided with a manometer. In FIGURE 2, the Pressure-Volume-Temperature cell comprises a metallic vessel able to withstand high pressure and temperature, mercury being  
15 used as a piston to vary pressure and volume of the petroleum oil contained in the interior of the vessel. In the above form of the invention, during the measurement of the wax appearance temperature, the gasmeter is substituted for the densimeter. The gasmeter is used only during the release of gas when the  
20 oil composition is to be changed. After the release of gas, the PVT cell is again connected to the densimeter, as explained in detail hereinafter with reference to Figure 3.

The preferred gas-containing petroleum oil for use with the Pressure-Volume-Temperature cell is an oil having the  
25 composition of a reservoir oil, the oil being collected either by bottom sampling by means of a special sampler within the well and near the reservoir face or on the surface by separately collecting the liquid and the separator gas on the surface and recombining them in the laboratory following the  
30 conditions of pressure, temperature and separation flowrates.

For the preferred embodiment of the invention which contemplates the presence of dissolved gas, the parameter Solubility ratio ( $S_r$ ) should be taken into consideration,  $S_r$  being the volume of gas dissolved per residual oil volume, at  
35 the considered pressure and temperature, both under standard conditions.

As illustrated in FIGURE 3, the method of the present invention which leads to the wax appearance point as a function of the solubility ratio  $S_r$  of a petroleum oil comprises, for

each Sr, the following steps:

- transferring to the Pressure-Volume-Temperature cell a typical reservoir petroleum oil sample at a pressure higher than the saturation pressure (bubble pressure) and without
- 5 altering the temperature of the sample, the volume of the sample being at least 30 cm<sup>3</sup> for each desired depletion stage;
- heating the Pressure-Volume-Temperature cell 1 to the reservoir temperature;
- after reducing the pressure in the densimeter and the steel
- 10 lines which link the Pressure-Volume-Temperature to the densimeter, transferring a sample of the petroleum oil contained in the Pressure-Volume-Temperature cell 1 to the densimeter 2 through the heated steel lines in order to obtain the wax appearance point of the oil which contains the whole of
- 15 the dissolved gas;
- for each Solubility ratio, measuring the density, the densimeter readings being obtained every 10 minutes at intervals of 1°C. The reading of the period leads to the density by means of the densimeter calibration equation, as
- 20 described hereinbefore;
- after reading one Solubility ratio, disconnecting the densimeter 2 and the Pressure-Volume-Temperature cell 1, reducing the pressure in the cell by means of a mercury pump to below the bubble pressure, and agitating the cell so as to
- 25 attain equilibrium between the created gas phase and the liquid phase, the gas released by the cell 1 being transferred to a gasmeter 3 for measuring the volume under atmospheric conditions;
- reconnecting the densimeter 2 to the Pressure-Volume-
- 30 Temperature cell 1 in order to obtain a new density corresponding to a new Solubility ratio, feeding the densimeter cell with an oil which has been depleted of a certain volume of gas, and measuring the wax appearance point of this gas-depleted petroleum oil;
- 35 - repeating the procedure for measurement of the density, disconnecting the Pressure-Volume-Temperature cell 1, effecting gas depletion, reconnecting the Pressure-Volume-Temperature cell 1 to the densimeter 2, and again measuring the density so that after successive stages of depletion the petroleum oil is

completely deprived of the originally contained gas, so that the oil is at atmospheric pressure, which is the condition for the measurement of the wax appearance point of the dead oil.

Readings of the position of the mercury pump lead to values for the volume of oil present within the Pressure-Volume-Temperature cell 1 at each depletion stage as well as to the volumes transferred to the densimeter 2. From the volumes of liquid and the volumes of gas released at each depletion stage it is possible to determine the Solubility ratio  $S_r$  (volume of gas dissolved in the oil) for the oils formed at each depletion stage.

The present invention will be now illustrated by the following Example, which should not be construed as limiting it.

#### EXAMPLE

The Barracuda oil field is a giant oil field under exploration by the Brazilian State Oil Company PETROBRAS, the oil field being located at the Campos Basin, in the State of Rio de Janeiro, at a water depth between 600 and up to 1200 meters. The subsea lines used to carry the oil production from the wellhead placed on the sea bottom and up to the platform encounter temperatures as low as 4°C. The oil which leaves the reservoir at 2960 meters depth has a temperature of 86.1°C and is cooled throughout the process of being passed along the well and the subsea lines. The temperature gradient of the hydrocarbon fluid depends chiefly on its production flowrate and on the temperature outside the line. In the case of long lines, the fluid temperature can be lowered to the temperature of the sea bottom. In order to point out any plugging which might occur in the lines caused by paraffinic deposits, as well as the position of the line where the deposit could occur, the temperature of the petroleum oil at each position should be compared to the wax appearance point of the same oil under the corresponding condition of pressure and flow temperature. Besides the decrease in temperature, a pressure decrease is also noticed along the line with the consequent gradual release of the gas dissolved in the reservoir fluid, the final condition being that of dead oil (without dissolved gas) which

is stored under atmospheric pressure. Note that the use of the wax appearance point of the dead oil (which is the more critical condition for paraffins) for indicating the occurrence of precipitation throughout the whole extent of the line can lead to non-representative results. Therefore, under these circumstances it is imperative to determine the wax appearance point under the flow conditions. In order to associate the flow condition of the hydrocarbon fluid to the wax appearance point, an experiment was run combining a Pressure-Volume-Temperature cell (which is a metallic vessel able to withstand high pressure and temperature and which uses mercury as a piston in order to vary the pressure and volume of the sample under study) to a digital densimeter, also adapted to withstand high pressure and temperature so as to measure the wax appearance point using the method of the present invention.

In this Example a petroleum oil in the reservoir condition was sampled from the well depth, at the face of the producing interval. In this kind of sampling the petroleum oil which is collected contains the whole of the solubilized gas. The sampling was made at the 3-BR-2-RJS well on June 7, 1993. The following procedure was used to obtain the experimental data:

a) the as-collected hydrocarbon fluid from the reservoir was transferred to the Pressure-Volume-Temperature cell at 350 kgf/cm<sup>2</sup> at a temperature of 86.1°C;

b) by withdrawing mercury from the Pressure-Volume-Temperature cell the pressure of the fluid was carefully reduced until the appearance of the first gas bubble (bubble pressure or saturation pressure).

The experimental value found for the bubble pressure was 138.5 kg/cm<sup>2</sup> at 86.1°C;

c) under this saturation condition, with all the gas dissolved, a first portion of the petroleum oil is transferred to the densimeter, where a wax appearance point of 11°C is determined;

d) pressure is then reduced to 120.0 kgf/cm<sup>2</sup> which is lower than the bubble pressure, this leading to a gas phase. Once the gas-liquid equilibrium has been attained, the gas phase is integrally transferred to a gasmeter, where the volume of gas can be accurately metered under atmospheric conditions. This

volume is then corrected to standard conditions (15.6°C and 760 mm Hg) so as to define a volume  $V_1$ ;

e) under a pressure of 120.0 kgf/cm<sup>2</sup>, a portion of the depleted oil is transferred to the densimeter which has been connected

5 to the top of the Pressure-Volume-Temperature cell. The new value for the wax appearance point is 13°C;

f) Steps d) and e) are repeated at pressures (gauge) of 100.00 kgf/cm<sup>2</sup>, 80.0 kgf/cm<sup>2</sup>, 40.0 kgf/cm<sup>2</sup>, 20.0 kgf/cm<sup>2</sup> and finally at atmospheric pressure (dead oil). At steps d) gas volumes named

10  $V_2$ ,  $V_3$ ,  $V_4$ ,  $V_5$  and  $V_6$  are measured, corresponding to depletion pressures (gauge) of 100, 80, 40, 20 and 0.0 kgf/cm<sup>2</sup>

respectively. The residual oil volume in the Pressure-Volume-Temperature cell, as measured in the standard conditions 15.6°C and 760 mm Hg, is the reference volume for calculating the

15 solubility ratio  $S_r$ . By definition, the solubility ratio at atmospheric pressure is zero. The solubility ratio at 20.0 kgf/cm<sup>2</sup> pressure (gauge) is calculated by dividing the volume

( $V_6$ ) of gas which left solution during the reduction in pressure from 20.0 kgf/cm<sup>2</sup> to zero by the volume ( $V_r$ ) of

20 residual oil, that is,  $S_r(20.0) = V_6/V_r$ . If, at the pressure (gauge) of 20.0 kgf/cm<sup>2</sup>, oil from the cell has not been supplied to the densimeter, the Solubility ratio at 40.0

kgf/cm<sup>2</sup> would be calculated by dividing the total volumes of gas which had left solution during reductions in pressure from

25 20.0 kgf/cm<sup>2</sup> to zero and from 40.0 kgf/cm<sup>2</sup> to 20.0 kgf/cm<sup>2</sup> by the volume of residual oil:  $S_r(40.0) = (V_5 + V_6)/V_r$ . This

procedure should be successively repeated up to the bubble pressure, for which the Solubility ratio would be calculated by dividing the total volume of released gas ( $V_1+V_2+V_3+V_4+V_5+V_6$ )

30 by the volume of residual oil, which is the definition of the overall Solubility ratio of the oil. However, in view of

additional intermediate oil withdrawals, the complexity attained by the calculations requires software to be adequately

written. Note that every volume of oil transferred to the

35 densimeter has a volume of dissolved gas which is not measured in the gasmeter.

TABLE 1 and FIGURE 6 show the results obtained for a petroleum oil from the 3-BR-2-RJS well, which contains 3.3 wt % of paraffins, according to the Shell Method Series 1769-88. In

column 1 are tabulated the figures for the pressure where the gas was released from the Pressure-Volume-Temperature cell to the gasmeter, and the resulting fluid (petroleum oil) in the cell transferred to the densimeter in order to measure the wax appearance point. Column 2 presents the figures for Solubility ratio  $S_r$  which is the volume of gas kept in solution at each pressure stage. The third column lists the figures of wax appearance point determined in the densimeter.

TABLE 1

	Pressure kgf/cm <sup>2</sup>	$S_r$ m <sup>3</sup> /m <sup>3</sup>	Wax appearance point °C
15	138.5	65.07	11
	120.0	57.84	13
	100.0	50.54	15
20	80.0	42.96	17
	40.0	27.35	20
25	20.0	18.58	22
	0.0	0.0	25

In order to represent the linear behaviour of the experimental points, a straight line equation was determined using a linear regression statistical software:

$$\text{Wax appearance point} = 25.5 - 0.215 S_r$$

wherein the correlation coefficient is  $R^2 = 0.99$ , that is, a nearly perfect straight line.

Using the inventive method, wax appearance point measurements were effected for dissolved gas-containing reservoir oils of various wax contents. The linear behaviour for wax appearance point vs. solubility ratio  $S_r$  was repeated for various other oils.

In view of the fact that the difference in wax appearance point between dead oil and dissolved gas-containing oils can be significant, the process of the present invention constitutes an important contribution to the technique of wax appearance point measurement, mainly in the area of dissolved gas-containing oils.

Note that, among the prior art methods for the measurement of the wax appearance point of dead oil, only the method based on the viscosity change as a function of temperature could be used for the measurement of the wax appearance point of dissolved gas-containing hydrocarbon fluids. However, viscometers such as those of the Rolling Ball type which are normally used in petroleum oil analyses and which infer the viscosity of solubilized gas-containing hydrocarbon fluids through the measurement of the time of fall of an iron sphere, are low-precision instruments which cannot identify the change in the viscosity behavior of low wax content petroleum oils. Besides, in these viscometers, although petroleum oils can be heated, they cannot be cooled to sub-ambient temperatures.

Still, as relates to the relationship between the present application and the prior art methods, British GB-A-2268276 as well as the present application are both based on the measurement of the reduction in volume undergone by a hydrocarbon fluid sample as a consequence of a temperature reduction. At the temperature of the onset of wax precipitation, the contraction in volume undergone by the hydrocarbon fluid is stronger, a deviation being observed from the contraction behaviour prior to precipitation. Then, this phenomenon is used to determine the wax appearance point, the precision of the measurement being directly related to the experimental accuracy of measuring variations in volume of the sample which could first indicate the occurrence of wax precipitation. However, the method to determine the wax appearance point according to GB-A-2268276 and the method disclosed in the present application are profoundly different. In the technique disclosed in the British publication, the hydrocarbon fluid, whose wax appearance point is to be determined, is kept within a metallic vessel and the volume contraction of the sample due to the wax precipitation is measured by way of a high pressure volumetric pump. It is hypothesized that the precision of such measurement is below the requirements for determining the wax appearance point of hydrocarbon fluids of low wax content. This can be inferred from the data of Figure 2 of GB-A-2268276, where it can be seen

that for a 60 cm<sup>3</sup> sample the smallest volume contraction to be determined is 0.017% of the total volume, since the accuracy of the volumetric pump is 0.01 cm<sup>3</sup> ( $0.01 \times 100\% : 60 \text{ cm}^3 = 0.017\%$ ). It occurs that this figure is related to the initial wax precipitation of hydrocarbon fluids of high wax content. Thus the method described in GB-A-2268276 seems limited to be applied to hydrocarbon fluids of a rather high wax content, this limitation being overcome by the method described and claimed by the present invention. The high precision of the present method results from the fact that the volume variation of the sample (fluid contraction) is measured by means of the density variation at constant mass. The density is measured by the natural oscillation frequency of the fluid, the accuracy being to the fourth decimal place for a volume of only 1.0 cm<sup>3</sup>, so that the wax appearance point of low wax content oils can be determined; for example a wax content below 1 wt %, as is the case for petroleum oils from the Marlim oil field of the Campos Basin, Rio de Janeiro, Brazil.

FIGURE 5 illustrates the inventive method for an oil containing as low as 0.5 wt % wax. The measurement of the wax appearance points of such petroleum oil using the prior art methods would be difficult and would show a rather large deviation from the real figure, since these methods lack the necessary accuracy for evaluating the wax appearance point of paraffinic oils of low wax content.

The method and apparatus of the present application also constitute an improvement regarding the way of determining the influence of the fluid composition on the wax appearance point. In this determination the composition of the fluid under study is varied by gradually withdrawing the dissolved gas. In the apparatus described in GB-A-2268276 several 60 cm<sup>3</sup> samples having different amounts of dissolved gas are transferred one at a time to the metallic vessel in which the wax appearance point is to be determined. Thus, in order to determine the influence of the fluid composition on the wax appearance point at least 1000 cm<sup>3</sup> of sample are needed, the petroleum oil being recombined under pressure with varying amounts of dissolved gas.

In the arrangement set forth in the present application,



the wax appearance points of various mixtures having different concentrations of dissolved gas are measured by coupling a Pressure-Volume-Temperature cell to the densimeter. The mixtures are prepared in the cell and transferred to the  
5 densimeter to determine the wax appearance point. In the method described and claimed herein, the Pressure-volume-Temperature cell is supplied with the reservoir hydrocarbon fluid (original mixture) and the subsequent mixtures result from the withdrawal of a portion of gas from such fluid. Thus,  
10 differently from the prior art methods, which require volumes of up to 1000 cm<sup>3</sup>, the process of the present invention requires samples of no more than 200 cm<sup>3</sup>, the various mixtures being obtained with a high degree of accuracy which reduces the experimental work and further speeds the collection of  
15 experimental data.

C L A I M S

1. A method for determining the wax appearance temperature of paraffinic petroleum oils, comprising measuring  
5 and plotting the density of the petroleum oil as a function of the temperature at constant pressure, and determining the wax appearance point as the temperature at which there is an inflexion in the graph.

2. A method according to claim 1, wherein density  
10 measurements are effected for different amounts of dissolved gas so as to determine the variation in the wax appearance temperature as a function of the Solubility ratio, where the solubility ratio is the ratio of the volume of gas dissolved at the test pressure and reservoir temperature to the volume of  
15 residual oil, both measured under standard conditions.

3. A method for determining the wax appearance temperature of paraffinic oils, substantially as hereinbefore described with reference to the accompanying drawings.

4. An apparatus for the measurement of the wax  
20 appearance temperature of paraffinic petroleum oils by the method according to claim 1 or 2, which comprises a bottle to contain the sample of paraffinic oil, a mercury pump for evacuating the bottle and a high pressure and temperature densimeter connected to the bottle for determining the  
25 variation in density of the sample with the temperature reduction, wherein the densimeter has its temperature regulated by an ultrathermostatic bath, and wherein the bottle, the mercury pump and the densimeter are connected together by a valve system.

30 5. An apparatus according to claim 4, wherein the bottle contains dead petroleum oil.

6. An apparatus according to claim 4, wherein the bottle contains petroleum oil with dissolved gas.

7. An apparatus according to claim 4, 5 or 6, wherein  
35 the bottle is a Pressure-Volume-Temperature cell which uses mercury as a piston to vary the pressure and the volume of the petroleum oil contained within the cell.

8. Apparatus for determining the wax appearance temperature of paraffinic petroleum oils, substantially as

hereinbefore described with reference to, and as illustrated in, the accompanying drawings.



Application No: GB 9601576.3  
Claims searched: ALL

Examiner: Michael Walker  
Date of search: 10 April 1996

## Patents Act 1977 Search Report under Section 17

### Databases searched:

UK Patent Office collections, including GB, EP, WO & US patent specifications, in:

UK Cl (Ed.O): G1S (SQA)

Int Cl (Ed.6): G01N 25/02, 25/12, 33/26, 33/28, 33/30

Other: On-line : WPI

### Documents considered to be relevant:

Category	Identity of document and relevant passage	Relevant to claims
X	GB 2268276 A (NORSK) page 4, ll.9-17; page 6, ll.9 etc	1
A,E	WO 95/20153 A1 (NESTE OY) see abstract	1

X Document indicating lack of novelty or inventive step  
Y Document indicating lack of inventive step if combined with one or more other documents of same category.  
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A Document indicating technological background and/or state of the art.  
P Document published on or after the declared priority date but before the filing date of this invention.  
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